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Please find below and/or attached an Office communication concerning this application or proceeding.

The time period for reply, if any, is set in the attached communication.

	Application No.	Applicant(s)
	10/586,781	JACOBSEN ET AL.
Office Action Summary	Examiner	Art Unit
	Brieann R. Fink	1763
The MAILING DATE of this communication app Period for Reply	pears on the cover sheet with the	correspondence address
A SHORTENED STATUTORY PERIOD FOR REPL WHICHEVER IS LONGER, FROM THE MAILING D - Extensions of time may be available under the provisions of 37 CFR 1.1 after SIX (6) MONTHS from the mailing date of this communication. - If NO period for reply is specified above, the maximum statutory period Failure to reply within the set or extended period for reply will, by statute Any reply received by the Office later than three months after the mailing earned patent term adjustment. See 37 CFR 1.704(b).	ATE OF THIS COMMUNICATION (36(a). In no event, however, may a reply be will apply and will expire SIX (6) MONTHS from (6), cause the application to become ABANDON	DN. timely filed m the mailing date of this communication. IED (35 U.S.C. § 133).
Status		
 1) ■ Responsive to communication(s) filed on 13 D 2a) ■ This action is FINAL. 2b) ■ This 3) ■ Since this application is in condition for allowa closed in accordance with the practice under B 	s action is non-final. nce except for formal matters, p	
Disposition of Claims		
4) ☑ Claim(s) 12-18 and 20-22 is/are pending in the 4a) Of the above claim(s) is/are withdra 5) ☐ Claim(s) is/are allowed. 6) ☑ Claim(s) 12-18 and 20-22 is/are rejected. 7) ☐ Claim(s) is/are objected to. 8) ☐ Claim(s) are subject to restriction and/or	wn from consideration.	
Application Papers		
9) The specification is objected to by the Examine 10) The drawing(s) filed on is/are: a) acc Applicant may not request that any objection to the Replacement drawing sheet(s) including the correct 11) The oath or declaration is objected to by the Example 11.	epted or b) objected to by the drawing(s) be held in abeyance. So tion is required if the drawing(s) is o	ee 37 CFR 1.85(a). bjected to. See 37 CFR 1.121(d).
Priority under 35 U.S.C. § 119		
12) Acknowledgment is made of a claim for foreign a) All b) Some * c) None of: 1. Certified copies of the priority document 2. Certified copies of the priority document 3. Copies of the certified copies of the prio application from the International Burea * See the attached detailed Office action for a list	ts have been received. ts have been received in Applica rity documents have been receiv u (PCT Rule 17.2(a)).	ution No ved in this National Stage
Attachment(s)		
1) Notice of References Cited (PTO-892) 2) Notice of Draftsperson's Patent Drawing Review (PTO-948) 3) Information Disclosure Statement(s) (PTO/SB/08) Paper No(s)/Mail Date	4) Interview Summal Paper No(s)/Mail I 5) Notice of Informal 6) Other:	Date

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DETAILED ACTION

1. This office action follows a reply filed on December 13, 2010. Claims 12 and 20-21 have been amended. Claims 12-18 and 20-22 are currently pending and under examination.

- 2. All previous rejections are withdrawn, as applicants have amended to include specific catalysts. However, upon further consideration, a new ground(s) of rejection is proposed below.
- 3. The texts of those sections of Title 35 U.S. Code are not included in this section and can be found in a prior Office action.

Claim Rejections - 35 USC § 102

4. Claims 12-15 and 18 are rejected under 35 U.S.C. 102(b) as being anticipated by *DeChellis* (US 5,405,922).

DeChellis discloses polymerizing olefins, preferably ethylene with an alpha-olefin comonomer having most preferably 5 to 10 carbon atoms, in the presence of a metallocene catalyst in a gas phase fluidized bed polymerization reactor operating in condensed mode (col. 3, II. 7-15, II. 27-33). DeChellis discloses the catalyst as being represented by the formula [L]_mM[X]_n, where L is a bulky ligand, specifically a cyclopentadienyl ligand, M is a transition metal, that of which is exemplified as zirconium, X is a leaving group and m and n are such that the total ligand valency corresponds to the transition metal valency (col. 4, II. 1-14, Examples, col. 9-10). DeChellis further discloses the fluidized bed as

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having a recycle stream separate from the fluidized bed, which is the reaction zone (col. 8, II. 29-35). *DeChellis* discloses that the recycle stream is compressed and/or cooled to form a liquid phase and a gas phase, which are reintroduced into the reactor (col. 2, II. 53-56). Further, *DeChellis* discloses maintaining at least a 5.6°C temperature differential between the dew point temperature and the reactor temperature (col. 6, I. 66-col. 7, I. 3). *DeChellis* discloses that the reactor pressure is most preferably in the range of about 250-350 psig, which is the same as 1.7-2.4 MPa, and a temperature in the range of 73.9-85°C (col. 8, II. 44-60). This falls within the preferred reaction conditions of the instant invention (see instant specification, p. 3, II. 22-23). *DeChellis* exemplifies polymerizing ethylene and octene, wherein the ratio of octene/ethylene is 0.0090 (Table 2 and 3, col. 11-12).

DeChellis fails to specifically disclose maintaining the partial pressure of the alpha-olefin at an amount to prevent condensation within the reactor; however, the amount of comonomer, reactor temperature and partial pressures in the reaction zone are clearly disclosed by DeChellis and the polymerization is also disclosed as being operated in "condensed mode". This is the same as the instant invention as described above. Therefore, the process of DeChellis inherently prevents condensation within the reactor, as required by the instant claim 12. This is further supported by the applicants' disclosure that "the level of condensation in the reactor...is controlled by the amount of comonomer and the

temperature and partial pressure in the reaction zone" (see arguments submitted May 26, 2009, page. 8).

As to claim 13, *DeCellis* discloses the partial pressure of ethylene as between 75-240 psig, which is the same as 0.5-1.6 MPa. (col. 6, II. 14-20).

As to claims 14-15, *DeChellis* exemplifies the polymerization of ethylene and octene the ratio of octene/ethylene is 0.0090 (Table 2 and 3, col. 11-12).

As to claim 16, *DeCellis* discloses the alpha-olefins to include those having 5 to 10 carbon atoms (col. 3, II. 33), wherein that having 10 carbon atoms is 1-decene.

As to claim 18, *DeChellis* discloses the process as continuous (col. 1, II. 9-10).

Claim Rejections - 35 USC § 103

5. Claims 20 and 22 are rejected under 35 U.S.C. 103(a) as being unpatentable over *DeChellis* (US 5,405,922), as applied above to claims 12-16 and 18, in view of *Nickias* (WO 93/08199).

DeChellis discloses the claimed method of instant claims 12-16 and 18, as described above and applied herein, teaching the metallocene catalysts as being represented in general as described above and claimed in instant claim 12, specifically listing other catalysts and catalyst systems to include those as disclosed by *Nickias*, WO 93/08199 (col. 4, II. 64-67).

Nickias teaches the same catalysts as claimed in instant claim 20 (p. 4-5).

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Therefore, it would have been obvious to one of ordinary skill in the art at the time the invention was made to have carried out the method of polymerization of *DeChellis* using the catalysts of *Nickias* as *DeChellis* specifically discloses these catalysts as being useful.

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As to claim 22, *Nickias* teaches titanium as a most preferred metal (p. 5, I. 16).

6. Claims 21 is rejected under 103(a) as being unpatentable over *DeChellis* (US 5,405,922), as applied above to claims 12-16 and 18, in view of *Nickias* (WO 93/08199), as evidenced by *Wilson* (US 5,659,054), and further in view of *Devore* (US 5,470,993).

DeChellis discloses the claimed method of instant claims 12-16 and 18, as described above and applied herein, teaching the metallocene catalysts as being represented in general as described above and claimed in instant claim 12, specifically listing other catalysts and catalyst systems to include those as disclosed by *Nickias*, WO 93/08199 (col. 4, II. 64-67).

Nickias exemplifies the catalyst as (N-t-butylamido)dimethyl(tetramethylη⁵-cyclopentadienyl)silanetitanium dibenzyl (p. 11, Example 4), which as
evidenced by Wilson is a titanium (+4) complex (col. 10, II. 32-34), as are all of
those disclosed by Nickias.

Devore teaches titanium and zirconium complexes which are the same as those claimed in instant claim 21 (col. 6, II. 16-50). Devore teaches these complexes to possess improved catalytic properties when compared to

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corresponding complexes wherein the metal in the +4 formal oxidation state, specifically that they retain high catalytic efficiency at elevated temperatures, give higher molecular weight polymers, are compatible with alkylaluminum compounds, and are more readily and efficiently activated by common activating cocatalysts, when compared to corresponding complexes wherein the metal in the +4 formal oxidation state.

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Therefore, it would have been obvious to one of ordinary skill in the art at the time the invention was made to have carried out the polymerization of *DeChellis* using the catalysts of *Devore* rather than titanium (+4) complexes of *Nickias* as *Devore* teaches these catalysts to have improved catalytic properties

Note the instant specification specifically discloses that "specific complexes suitable for use in the present invention are those disclosed in WO 95/00526, which is the same as US 5,470,993, *Devore*.

7. Claims 12-18, 20 and 22 rejected under 35 U.S.C. 103(a) as being unpatentable over *Agapiou* (US 7,244,795)

Agapiou teaches preparing a copolymer of ethylene, where the comonomer is an alpha-olefin having 4-14 carbon atoms, specifically listing 1-octene and 1-decene, in a continuous gas phase polymerization carried out in a fluid bed process having a reactor and a recycling stream, wherein the recycling comprises gaseous monomer and a diluent.

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Agapiou teaches the catalysts to include a variety of catalysts, most of which fall within the claimed formula, specifically those of formula (Va-ii), which are the same as those of instant claims 20 and 22 (col. 4-15).

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Agapiou teaches the reactor temperature as 30-150°C and a pressure of 250-350 psig (col. 23, II. 5-7 and col. 24, II. 34-40), which is the same as 1.7-2.4 MPa, which are the same conditions as those desired by the instant invention (see instant specification, p. 3, II. 18-21).

Agapiou fails to explicitly teach that the gas phase polymerization is operated in "condensed mode", as required by instant claim 12, however, applicants define "condensed mode" as "...the process of purposefully introducing a recycle stream having a liquid and a gas phase into the reactor ..." (see instant specification, p. 2, II. 23-31). Agapiou meets this definition and therefore operates in "condensed mode".

As to claims 14-17, Agapiou teaches the copolymerization of ethylene with an α-olefin comonomer having 4 to 14 carbons, specifically listing octene-1 and decene-1 as comonomers, and that of which are copolymerized in a mole ratio of comonomer to ethylene of from 0.0005 to 1.0 (col. 23, II. 40-50). This ratio is equivalent to the partial pressure ratio of comonomer to ethylene, which can be shown when applied to the ideal gas law (pV = nRT). This range overlaps the claimed range of claims 15 and 17, and it has been held that overlapping ranges are sufficient to establish *prima facie* obviousness. See MPEP 2144.05.

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Agapiou fails to specifically teach that the amount of α -olefin is maintained at a level at which to "prevent condensation" in the reactor; however, the amount of comonomer and temperature and partial pressures in the reaction zone are clearly taught by *Agapiou* and the polymerization is operated in "condensed mode", as described above.

Therefore, the process of *Agapiou* is inherently carried out such to "prevent condensation", as required by the instant claim 12. This is further supported by the applicants' disclosure that "the level of condensation in the reactor...is controlled by the amount of comonomer and the temperature and partial pressure in the reaction zone" (see arguments submitted May 26, 2009, page. 8 and instant specification, p. 3, II. 7-9).

Response to Arguments

8. Applicant's arguments with respect to the instant invention have been considered but are most in view of the new ground(s) of rejection.

Conclusion

9. Any inquiry concerning this communication or earlier communications from the examiner should be directed to Brieann R. Fink whose telephone number is (571)270-7344. The examiner can normally be reached on Monday through Friday, 7:00 AM to 4:30 PM (EST).

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If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Milton I. Cano can be reached on (571)272-1398. The fax phone number for the organization where this application or proceeding is assigned is 571-273-8300.

Information regarding the status of an application may be obtained from the Patent Application Information Retrieval (PAIR) system. Status information for published applications may be obtained from either Private PAIR or Public PAIR. Status information for unpublished applications is available through Private PAIR only. For more information about the PAIR system, see http://pair-direct.uspto.gov. Should you have questions on access to the Private PAIR system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free). If you would like assistance from a USPTO Customer Service Representative or access to the automated information system, call 800-786-9199 (IN USA OR CANADA) or 571-272-1000.

/Milton I. Cano/ Supervisory Patent Examiner, Art Unit 1763 /Brieann R Fink/ Examiner, Art Unit 1763